#### Notes for Assignment 2 Maths 323 fluids 2014

Last time: Continuity Equation (Sec 6-7) Force Balance (Sec 6-8) Stream Function (Sec 6-9) Postglacial Rebound (Sec 6-10) Angle of Subduction (Sec. 6-11) Diapirs intro (Sec 6-12)

#### Notes for Assignment 2 Maths 323 fluids 2014 Day 2

This time: Diapirs (Sec 6-12) Stokes Flow (Sec 6-14)

#### Equations so far

**Continuity Equation in 2D** 

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad \text{where} \quad 3\text{-D:} \\ u = \frac{\partial x}{\partial t}; v = \frac{\partial y}{\partial t}$$

$$\vec{\nabla} \cdot \vec{u} = 0$$

Balance of pressure and viscous forces

Eq(6-67) 
$$\frac{\partial P}{\partial x} = \mu (\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2})$$
 3-D:  $\nabla P = \mu \nabla^2 \vec{u}$   
Eq(6-68)  $\frac{\partial P}{\partial y} = \mu (\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2})$  Where P=p-pgy=deviatoric stress

$$u = -\frac{\partial \psi}{\partial y}; v = \frac{\partial \psi}{\partial x} \qquad \nabla^4 \psi = 0$$
$$Q = \int_A^B d\psi = \psi_B - \psi_A$$

Stream function  $\psi$ Biharmonic Equation:

Flow rate from integral of stream function

### Diapirs (Rayleigh-Taylor Instabilities) (not nappies)

- Driven by gravity and density imbalances—high over low
- Examples:
  - Paint dripping
  - Mantle "drips"
  - Start of convection, plumes, lava lamps
  - Salt domes
- Could grow exponentially until it breaks up, or could die out--returning to original state (but not periodic—not elastic)

#### Salt Domes





Images from : http://geology.com/stories/13/saltdomes/

#### Basic Eqn: Incompressible continuity Eqn $\vec{\nabla} \cdot \vec{u} = 0 \text{ or } \nabla^4 \psi = 0$

Balance Buoyancy Forces by Pressure Forces:



=0 if forces are in balance (e.g., eqn 6-151)

To solve eqn—introduce stream function  $\psi$  Like postglacial rebound or subducting plate—but boundary conditions differ

**6–21** The Rayleigh–Taylor instability of a dense fluid overlying a lighter fluid.



In general, b<sub>1</sub>≠b<sub>2</sub>

Displacement w<<  $b_1$  and  $b_2$ -- approximation is very important –i.e., Interface shape is w=Acos2 $\pi$ x/ $\lambda$ 

Because A is small, can treat interface as if it were at y=0 for the purposes of solving boundary conditions

- Boundary conditions:
  - 1)Rigid at top and bottom (-b<sub>1</sub> and b<sub>2</sub>)—no slip condition (u continuous)
  - $\therefore$  u=v=0 at y= -b<sub>1</sub> and b<sub>2</sub>
  - 2) Displacements and velocities and shear stress must be continuous across boundary between media (i.e., at interface, but since w is small, effectively y=0 here)

#### Guess solutions of $\boldsymbol{\psi}$

- $\psi_1$ ;  $\psi_2$  separate for each of top, bottom.
- $\psi$  is similar in form to postglacial rebound, but uses hyperbolic functions instead of simple sines and cosines:



#### Solve by:

- Show that both  $\psi_{1,2}$  are solns by substituting back into eqn,
- Determine  $u_{1,2}$  and  $v_{1,2}$  from derivatives of  $\psi_{1,2}$   $u_{1,2} = -\frac{\partial \psi_{1,2}}{\partial y}; v_{1,2} = \frac{\partial \psi_{1,2}}{\partial x}$
- Boundary conditions:
- u=v=0 at y= -b<sub>1</sub> and b<sub>2</sub> → u(x,y) become
   u<sub>1</sub>(x,-b<sub>1</sub>)=0; v<sub>1</sub>(x,-b<sub>1</sub>)=0
   u<sub>2</sub>(x,b<sub>2</sub>)=0; v<sub>2</sub>(x,b<sub>2</sub>)=0

**6–21** The Rayleigh–Taylor instability of a dense fluid overlying a lighter fluid.



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  - 1)Rigid at top and bottom (-b<sub>1</sub> and b<sub>2</sub>)—no slip condition (u continuous)
  - $\therefore$  u=v=0 at y= -b<sub>1</sub> and b<sub>2</sub>
  - 2) Displacements and velocities and shear stress must be continuous across boundary between media (i.e., at interface, but since w is small, effectively y=0 here)

#### 2) velocities and shear stress must be continuous across boundary between media (i.e., at y=0 here because w is small)

•  $u_1(x,0)=u_2(x,0); v_1(x,0)=v_2(x,0)$ 

$$\tau_{xy} = \mu(\frac{\partial u}{\partial y} + \frac{\partial v}{\partial x}) \text{ is same at boundary,}$$
$$\mu(\frac{\partial u_1(x,0)}{\partial y} + \frac{\partial v_1(x,0)}{\partial x}) = \mu(\frac{\partial u_2(x,0)}{\partial y} + \frac{\partial v_2(x,0)}{\partial x})$$

- (x dependence is purely a function of sin(2πx/λ))
- Another key—interface is moving with the same velocity as the fluid, so at y=0  $\frac{\partial w}{\partial t} = v(x,0)$

### Finally, balance forces--buoyancy and fluid flow pressure

6-22 The buoyancy force associated with the displacement of the interface.



$$(\rho_1 - \rho_2)gw = (P_2 - P_1)$$
 at y = 0

Flow pressure found from integrating 6-72

$$\frac{\partial P}{\partial x} = -\mu(\frac{\partial^3 \psi}{\partial x^2 \partial y} + \frac{\partial^3 \psi}{\partial y^3})$$

**Buoyancy** 

## Final solution after much algebra:

• Solution:

 $w = w_0 e^{t/\tau_a}$ 

- Where τ<sub>a</sub> is the growth time of the disturbance
- τ<sub>a</sub> (Eqn 6-158) is a function of sinh, cosh(2πb/λ) multiplied by

$$\frac{4\mu}{(\rho_2 - \rho_1)gb}$$

 $\tau_a$  depends on wavelength, but if have displacements at multiple wavelengths, fastest growing wavelength will dominate ( $\tau_a$  is a minimum)



# Stokes' Flow: How fast does a body fall due to its own weight?

- Applies in limit of very viscous fluid, with Re<1 (reversible flow)</li>
- Applications:
  - Fall of pieces of slab
  - Rise of plumes/magma
  - Fall of metal probe



Ball rises through stationary fluid or fluid flows past stationary ball



#### Sphere Falling in a Fluid



#### Sphere Falling in a Fluid



 $Fg + F_B + F_D = 0$ 



#### Fall of Iron into Core

Stevenson, David J. Mission to Earth's Core -A Modest Proposal. Nature, 423, 239-240, 2003. (in course notes)

About 1 week to get to core

#### Balance gravity (Buoyancy) and Viscous drag forces

• Dominant equations: continuity equation and pressure equation again, same as before but now geometry and boundary conditions change

$$\vec{\nabla} \cdot \vec{u} = 0 \qquad \vec{\nabla} P = \mu \nabla^2 u$$

- Where P=p-pgy
- $\rho_f$ =density of fluid
- $\rho_s$ =denisty of sphere

$$\operatorname{Re} = \frac{\rho_f U(2a)}{\mu}$$

![](_page_17_Figure_7.jpeg)

#### **Boundary Conditions**

• As  $r \rightarrow \infty$   $u_r \rightarrow -U$  in z direction  $u_r \rightarrow -U\cos\theta$   $u_{\theta} \rightarrow U\sin\theta$ No-slip on sphere: at r=a  $u_r = u_{\theta} = 0$ 

![](_page_18_Figure_2.jpeg)

#### **Spherical Coordinates:**

Continuity equation becomes:

$$0 = \vec{\nabla} \cdot \vec{u} = \frac{1}{r^2} \frac{\partial}{\partial r} (r^2 u_r) + \frac{1}{r \sin \theta} \frac{\partial}{\partial \theta} (u_\theta \sin \theta) + (\frac{1}{r \sin \theta} \frac{\partial u_\phi}{\partial \phi})$$

But since  $u_{\Phi}$ =0, last term is 0

To solve equation, also need the Laplacian of u:

$$\nabla^{2}\vec{u} = \vec{\nabla}(\vec{\nabla}\cdot\vec{u}) - \vec{\nabla}\times(\vec{\nabla}\times\vec{u})$$
$$\vec{\nabla}\times\vec{u} = \frac{1}{r\sin\theta} \left[\frac{\partial}{\partial\theta}(u_{\phi}\sin\theta) - \frac{\partial u_{\theta}}{\partial\phi}\right]\hat{r} + \frac{1}{r} \left[\frac{1}{\sin\theta}\frac{\partial u_{r}}{\partial\phi} - \frac{\partial(ru_{\theta})}{\partial r}\right]\hat{\theta} + \frac{1}{r} \left[\frac{\partial(ru_{\theta})}{\partial r} - \frac{\partial u_{r}}{\partial\theta}\right]\hat{\phi}$$

Pressure forces: Terms in P

Viscous forces: Terms in  $\mu \nabla^2 u$ 

#### Solution

- Surprisingly, most terms drop out and ...
- Pressure due to fluid flow is (Eq 6-216):

$$p = \frac{3\mu aU}{2r^2}\cos\theta$$

• Integrate to get downward "drag" (force) due to fluid pressure across sphere:  $D_p=2\pi\mu aU$ 

#### Viscous drag:

• Using 3-D formulation of stress again:

 $\vec{\tau} = \mu(\vec{\nabla}\vec{u} + \vec{\nabla}\vec{u}^T)$ 

Integrate to get Viscous Drag  $D_v=4\pi\mu aU$ So total Drag  $F_D$ = Viscous Drag + Pressure Drag =  $D_p$ +  $D_v=6\pi\mu aU$ 

#### Speed of rise or fall:

- Balance Buoyancy Forces with Drag forces for steady-state case (no acceleration):
- $F_B = (\rho_f \rho_s)g4\pi a^3/3 = F_D = 6\pi\mu aU$
- Solve for U

Pres

 For faster flow, Re>1, more difficult: use dimensionless drag coefficient C<sub>D</sub>

$$C_{D} = \frac{F_{D}}{\frac{1}{2}\rho_{f}U^{2}\pi a^{2}} = \frac{24}{\text{Re}}(6-226)$$
source due to vel. Sphere x-sec area (shado

![](_page_23_Figure_0.jpeg)

Note—units work out in both cases

#### Compare to pipe flow:

![](_page_24_Figure_1.jpeg)

![](_page_24_Figure_2.jpeg)

Depends on dimensionless variables: Friction factor *f* and Reynolds number *Re* 

$$f \equiv \frac{-4R}{\rho \overline{u}^2} \frac{dp}{dx}$$

![](_page_24_Figure_5.jpeg)